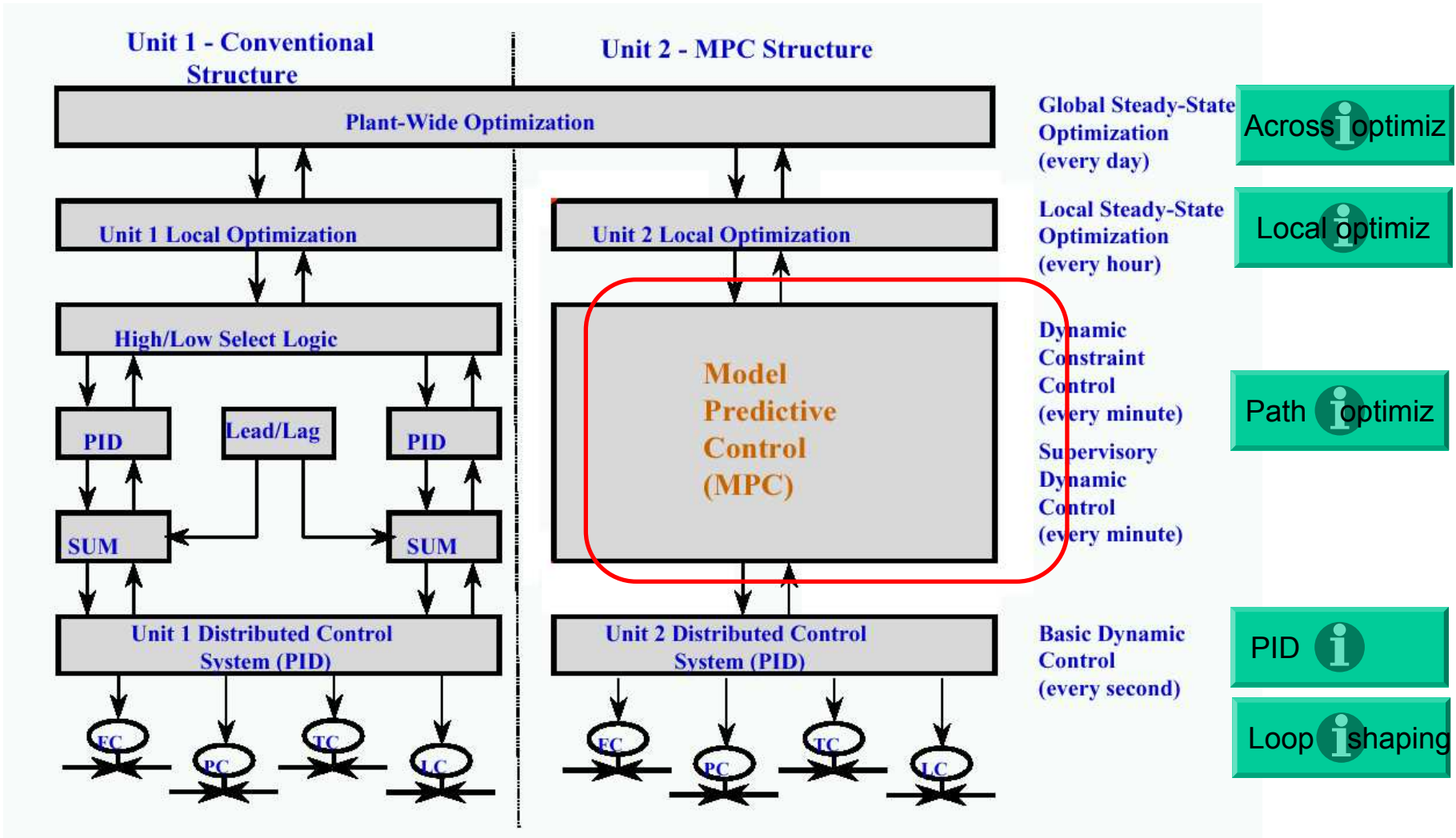


# Lecture 15 - Model Predictive Control

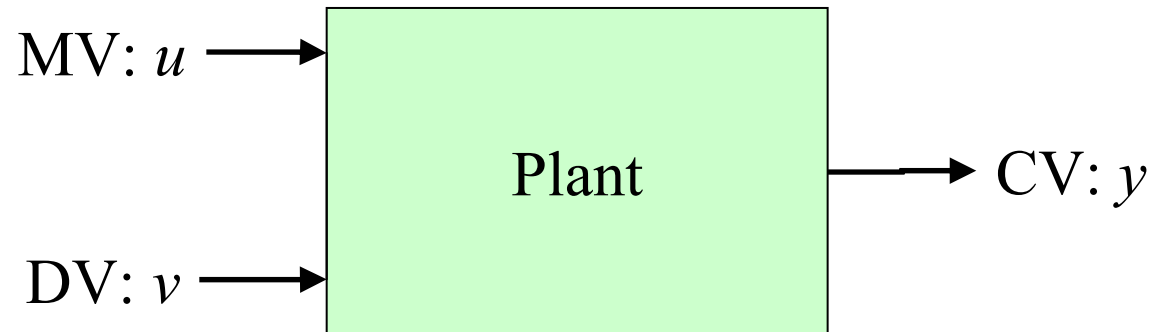
## Part 2: Industrial MPC

- Prediction model
- Control optimization
- Receding horizon update
- Disturbance estimator - feedback
- IMC representation of MPC

# Control Hierarchy



# MPC Setup



Plant structure:

- CV - controlled variables –  $y$ 
  - plant outputs, output errors
- MV - manipulated variables –  $u$ 
  - control inputs
- DV - disturbance variables -  $v$ 
  - disturbances and setpoints

# Models for MPC

- FIR (Finite Impulse Response) model
  - is used in some formulation
- FSR (Finite Step Response) model
  - Broadly used in process control

$$y(t) = \sum_{k=1}^n S^U(k) \Delta u(t-k) + \sum_{k=1}^n S^D(k) \Delta v(t-k) + d$$

- Compact notation

$$y(t) = (s^U * \Delta u)(t) + (s^D * \Delta v)(t) + d \quad \Delta = 1 - z^{-1}$$
$$h^U = \Delta s^U;$$

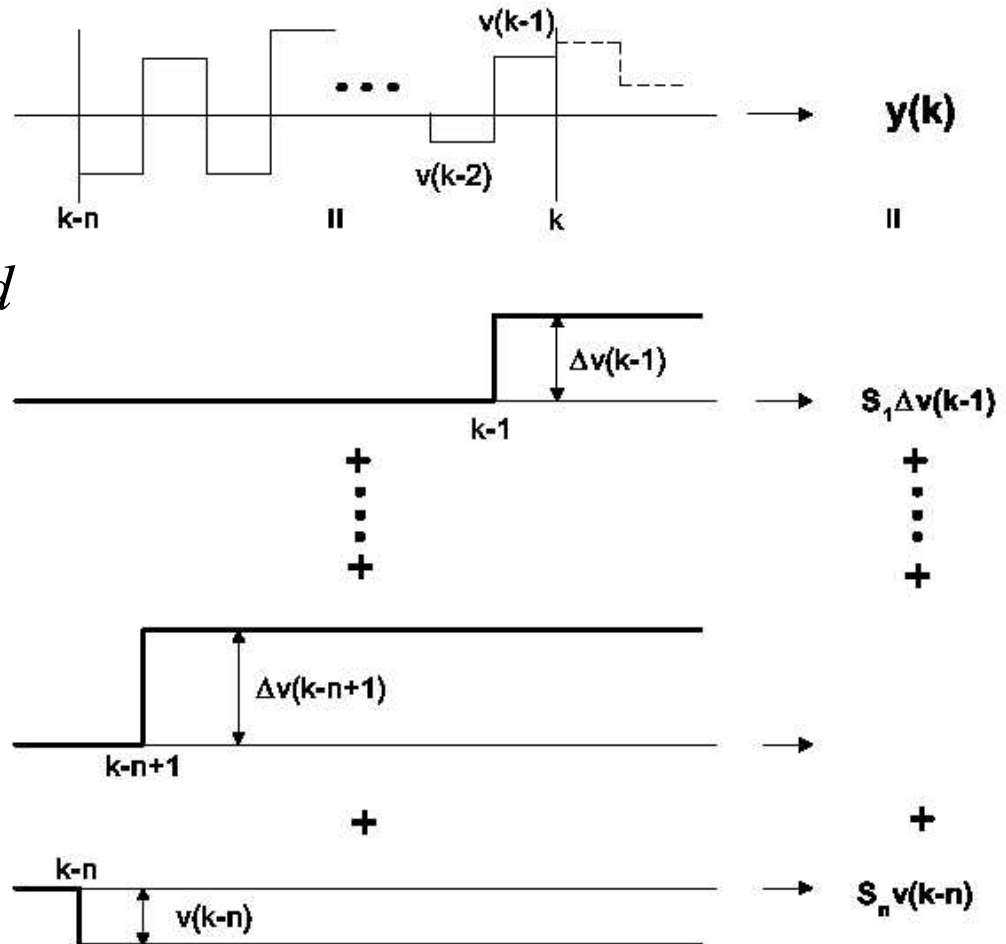
$$s^U * \Delta u = \Delta s^U * u = h^U * u$$

# Finite Step Response Model

FSR model

$$y(t) = \sum_{k=1}^n S(k) \Delta v(t-k) + d$$

- Ignores anything that happened more than  $n$  steps in the past
- This is attributed to a constant disturbance  $d$



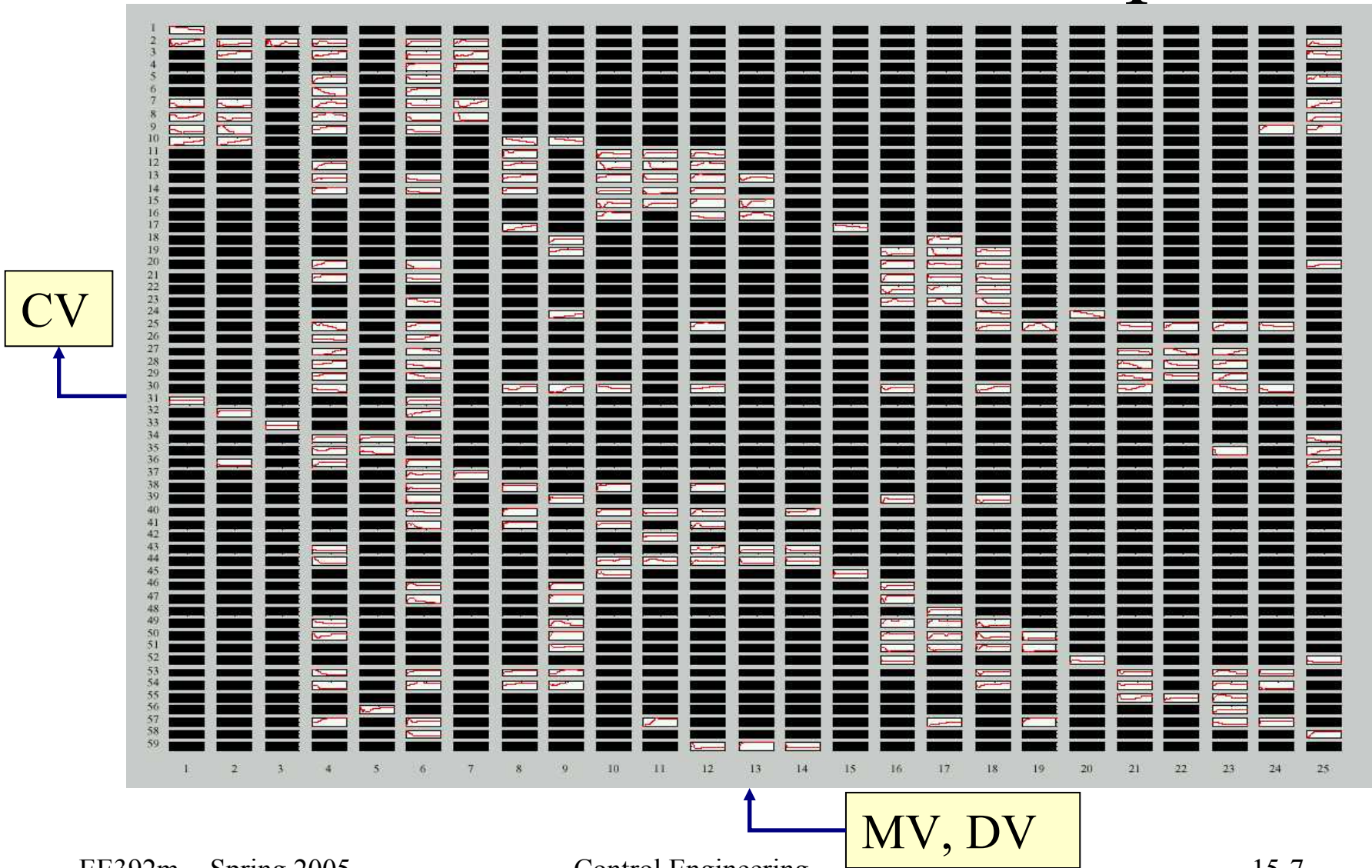
# MPC Model Identification

- Identification is a part of most industrial MPC packages
- Step (bump test) or PRBS

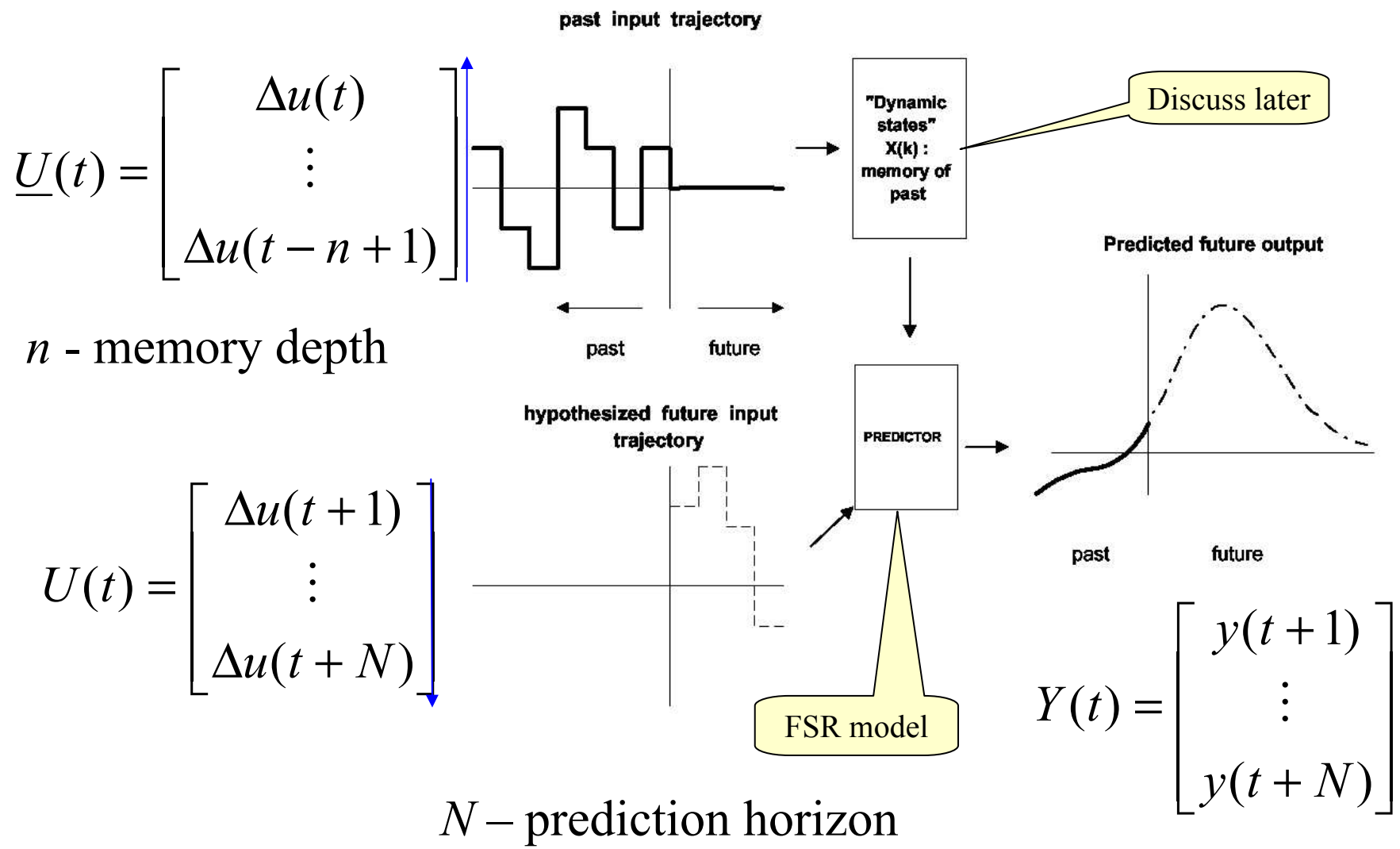
FIR model ID

- Step responses are directly used as models

# MPC Process Model Example



# Prediction Model





# System State for FSR Model

- MPC Concept

$$x(t) \rightarrow [\text{MPC Problem Solver}] \rightarrow u(t)$$

- FSR model state

$$x(t) = \begin{bmatrix} \underline{U}(t) \\ \underline{V}(t) \end{bmatrix}$$

- FSR model in state-space form

$$x(t+1) = Ax(t) + B^U \Delta u(t) + B^D \Delta v(t)$$

$$y(t) = Cx(t) + d$$

Past control moves

$$\underline{U}(t) = \begin{bmatrix} \Delta u(t) \\ \vdots \\ \Delta u(t-n+1) \end{bmatrix}$$

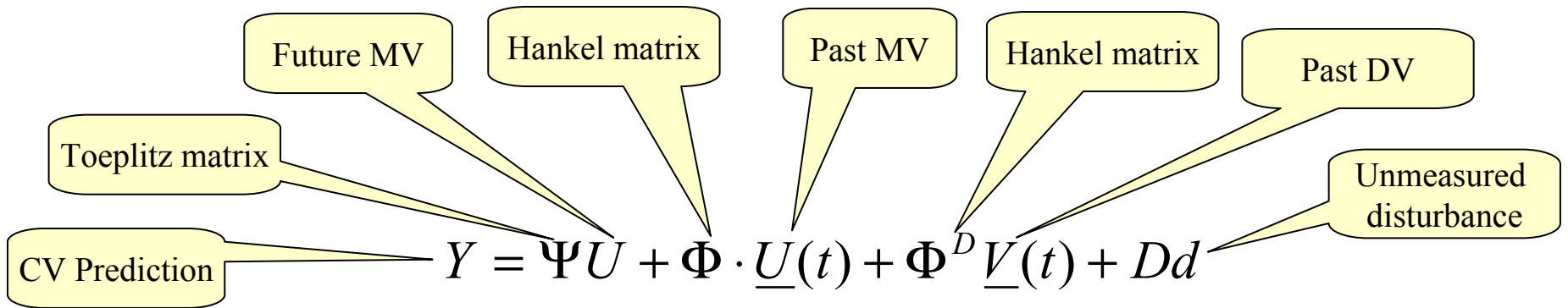
Past disturbances

$$\underline{V}(t) = \begin{bmatrix} \Delta v(t) \\ \vdots \\ \Delta v(t-n+1) \end{bmatrix}$$

Exercise: what are the matrices  $A, B^U, B^D, C$ ?

# Prediction Model

$$y(t) = (s^U * \Delta u)(t) + (s^D * \Delta v)(t) + d$$



$$\Psi = \begin{bmatrix} S^U(1) & 0 & \dots & 0 \\ S^U(2) & S^U(1) & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ S^U(N) & S^U(N-1) & \dots & 0 \end{bmatrix}$$

Toeplitz matrix

$$\Phi^D = \begin{bmatrix} S^D(2) & S^D(1) & \dots & S^D(n+1) \\ S^D(3) & S^D(2) & \dots & 0 \\ \vdots & \vdots & \ddots & \vdots \\ S^D(n+1) & 0 & \dots & 0 \end{bmatrix}$$

Hankel matrix

$$D = \begin{bmatrix} 1 \\ \vdots \\ 1 \end{bmatrix}$$

Future impact of the disturbance

# Optimization of Future Inputs

$$Y(t) = \Psi U(t) + \underbrace{\Phi \cdot \underline{U}(t) + \Phi^D \underline{V}(t) + Dd}_{Y^*(t)}$$

$Y^*(t)$  - free response of the system

- MPC optimization problem

$$J = Y^T(t) Q^Y Y(t) + U^T(t) R U(t) \rightarrow \min$$

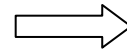
$$Q^Y = \begin{bmatrix} Q^y & \dots & 0 \\ \vdots & \ddots & \vdots \\ 0 & \dots & Q^y \end{bmatrix}, R = \begin{bmatrix} R^u & \dots & 0 \\ \vdots & \ddots & \vdots \\ 0 & \dots & R^u \end{bmatrix}$$

- Caveat: the problem might be ill-conditioned, then there is a need for regularization (an additional quadratic term in  $J$ )

# Optimization Constraints

- MV constraints

$$\begin{aligned} -\Delta u_{\max} &\leq \Delta u(t) \leq \Delta u_{\max} \\ u_{\min} &\leq u(t) \leq u_{\max} \end{aligned}$$

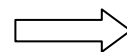


$$\begin{aligned} -\Delta u_{\max} &\leq U \leq \Delta u_{\max} \\ u_{\min} &\leq \Sigma U - C \leq u_{\max} \end{aligned}$$

$$u(t+k) = u(t) + \sum_{j=2}^k \Delta u(t)$$

- CV constraints

$$y_{\min}(t) \leq y(t) \leq y_{\max}(t)$$



$$Y_{\min} \leq Y \leq Y_{\max}$$

- Terminal constraint:

$$y(t+k) = 0; \quad \Delta u(t+k) = 0 \text{ for } k \geq p$$

# QP Solution

- QP Problem:

$$Aq \leq b$$

$$A_{eq}q = b_{eq}$$

$$J = \frac{1}{2}q^T Qq + f^T q \rightarrow \min$$

$$q = \begin{bmatrix} U \\ Y \end{bmatrix} \quad \begin{array}{l} \text{Decision vector:} \\ \text{predicted MVs, CVs} \end{array}$$

- Standard QP codes can be used

# Control Update

- System dynamics as an equality constraint in optimization

$$Y = \Psi U + Y^*(t)$$

Forced response

Free response

$$Y^* = [\Phi \quad \Phi^D] \cdot x(t) + d(t)$$

- Update of the system state

$$x(t+1) = Ax(t) + B^U \Delta u(t) + B^D \Delta v(t)$$

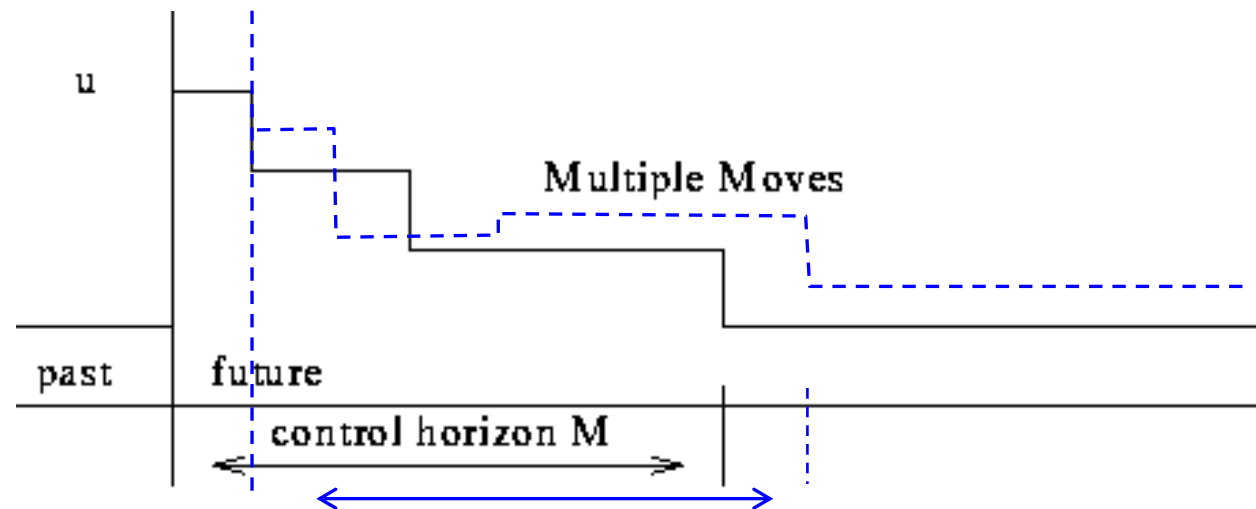
- Optimization problem solution at step  $t$  :

$$\{U_{OPT}, Y_{OPT}\} = \arg \min [J(U, Y)]$$

# Receding Horizon Control

- Use the first computed control value only
- Repeat at each  $t$

$$\Delta u(t+1) = [1 \quad 0 \quad \dots \quad 0] \cdot U_{OPT}(t)$$



# State Update and Estimation

- FSR model state update – delay line

$$x(t) = \begin{bmatrix} \underline{U}(t) \\ \underline{V}(t) \end{bmatrix} \quad \underline{U}(t) = \begin{bmatrix} \Delta u(t) \\ \vdots \\ \Delta u(t-n+1) \end{bmatrix} \quad \underline{V}(t) = \begin{bmatrix} \Delta v(t) \\ \vdots \\ \Delta v(t-n+1) \end{bmatrix}$$

- Disturbance estimator

$$d(t+1) = d(t) + k_I (y_m(t) - y(t))$$

Unmeasured disturbance

Actually observed CV

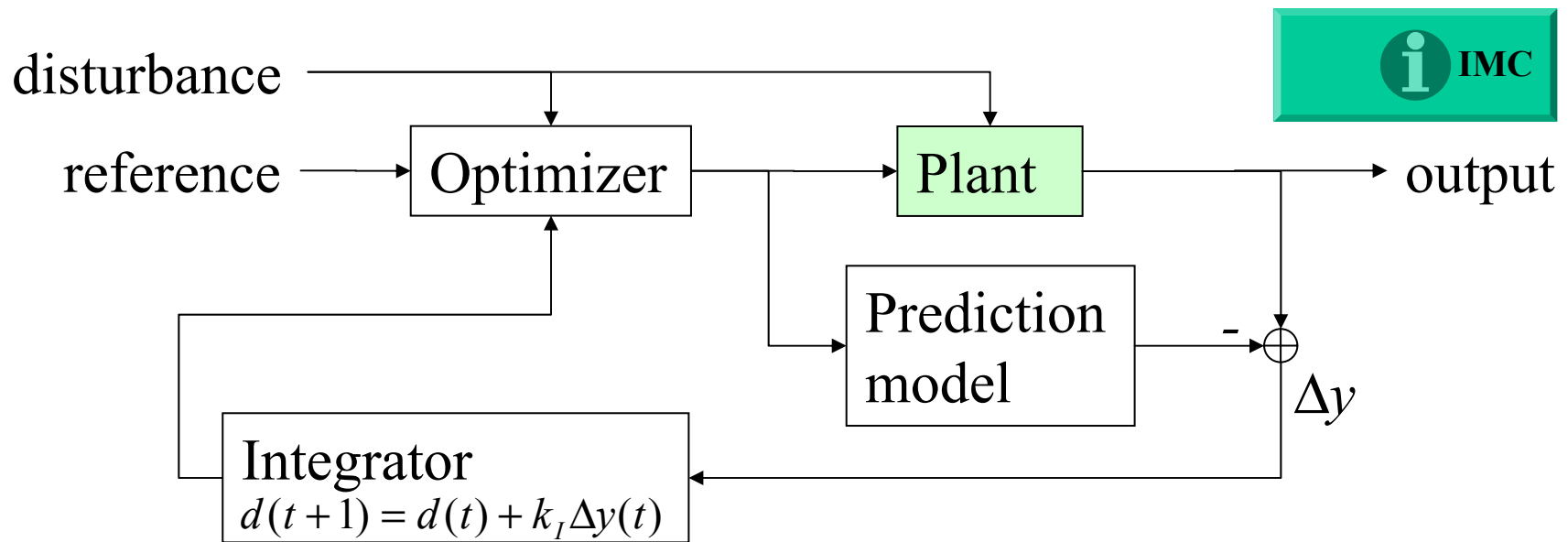
CV Prediction based on the current state  $x(t)$ .  
Computed at the previous step

- Disturbance estimator = Integrator feedback



# MPC as IMC

- MPC with disturbance estimator is a special case of IMC

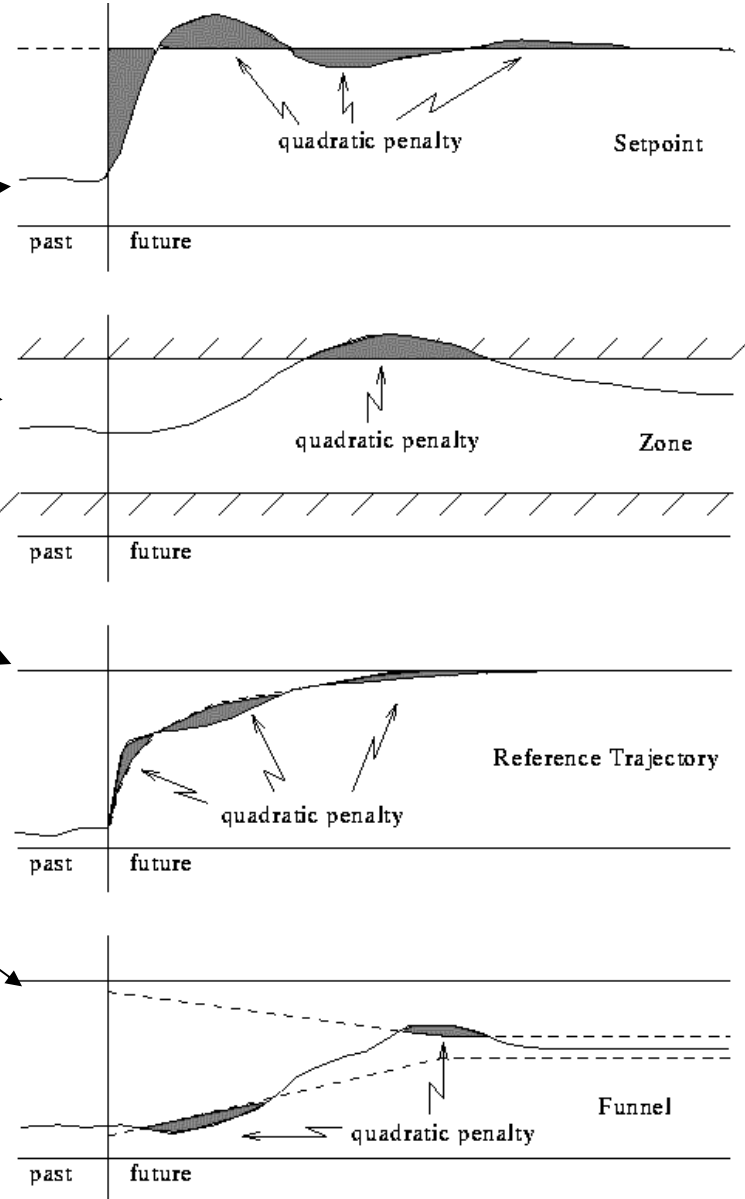


- Closed-loop dynamics (filter dynamics)
  - integrator in the disturbance estimator
  - $2n$  poles  $z = 0$  in the FSR model update



# Optimization detail

- Setpoint
- Zone
- Trajectory
- Funnel
- Soft constraints (quadratic penalties) and hard constraints for MV, CV
- Regularization
  - penalties
  - singular value thresholding



# Soft Constraints

- Consider a QP Problem

$$J = \frac{1}{2} x^T Q x + f^T x \rightarrow \min$$

subject to:  $Ax \leq b$

$A_s x \leq b_s$  soft constraint, might be infeasible

- Slack variable formulation:  $w = 0$  yields the original problem

Large penalty for constraint violation

$$J = \frac{1}{2} x^T Q x + \frac{1}{2} w^T S w + f^T x \rightarrow \min$$

subject to:

$$Ax \leq b$$

$$A_s x - b_s \leq w$$

$$0 \leq w$$

slack

$\begin{bmatrix} x \\ w \end{bmatrix}$  new augmented  
decision vector

# Industrial MPC Features

- Industrial strength products that can be used for a broad range of applications
- Flexibility to plant size, automated setup
- Based on step response/impulse response model
- On the fly reconfiguration if plant is changing
  - MV, CV, DV channels taken off control or returned into MPC
  - measurement problems (sensor loss), actuator failures
- Systematic handling of multi-rate measurements and missed measurement points
  - do not update the disturbance estimate  $d$  if the data is missing

# Technical detail

- Tuning of MPC feedback control performance is an issue.
  - Works in practice, without formal analysis
  - Theory requires
    - Large (infinite) prediction horizon or
    - Terminal constraint
- Additional tricks for
  - a separate static optimization step
  - integrating and unstable dynamics
  - active constraints
  - regularization
  - shape functions for control
  - different control horizon and prediction horizon
  - ...